

LECTURE

MODELLING THE MARINE ENVIRONMENT

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Lecture 9

STRETER- PHELPS MODEL

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- ❖ **Point source**
- ❖ **Distribution source**

STRETER- PHELPS POINT SOURCES

Mass balance equation:

$$\text{BOD:} \quad V \frac{dL}{dt} = -k_d VL$$

$$\text{DO:} \quad V \frac{do}{dt} = -k_d VL + k_a V(o_s - o)$$

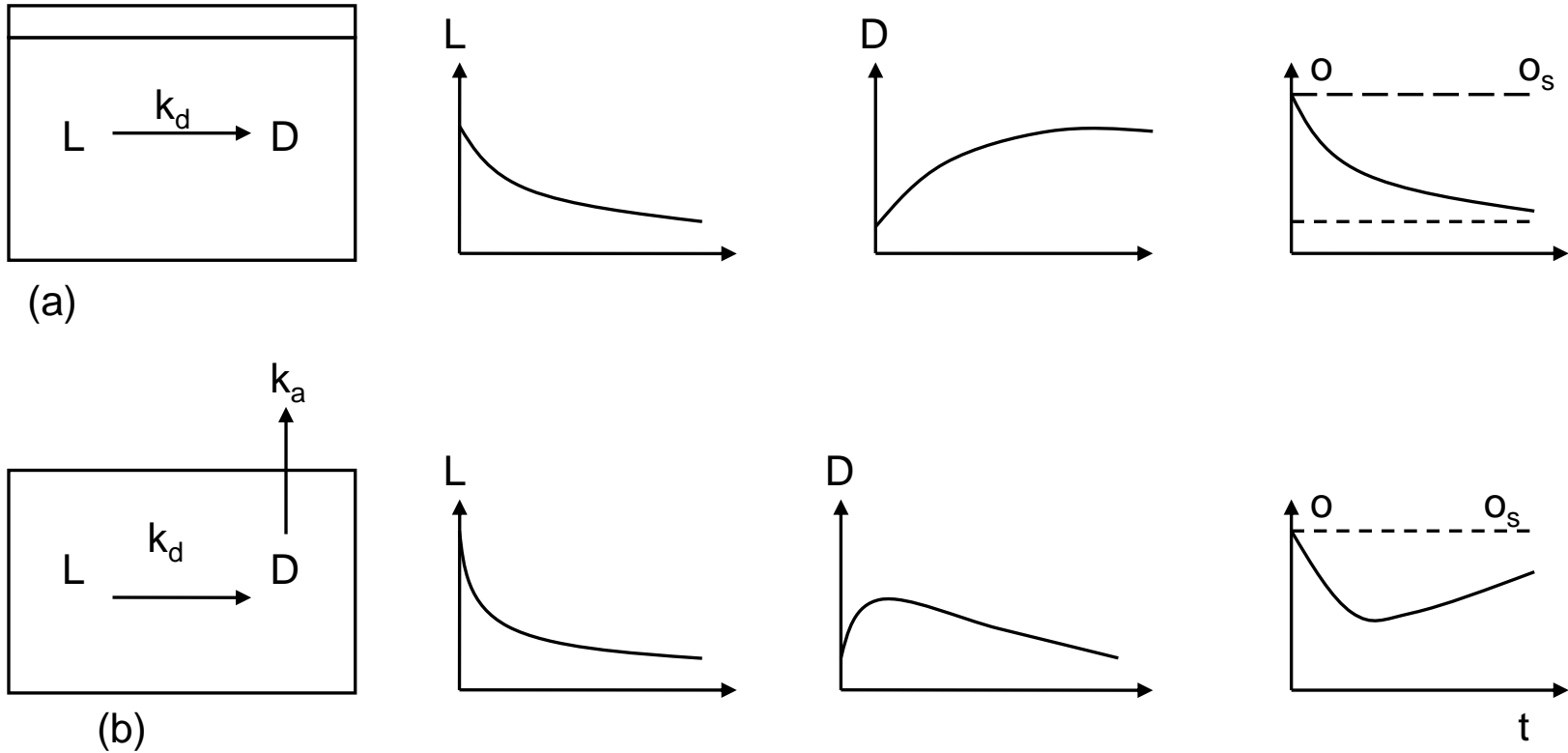
$$\text{DO Deficit: } D = o_s - o \quad \longrightarrow \quad \frac{dD}{dt} = -\frac{do}{dt}$$

$$\longrightarrow \quad V \frac{dD}{dt} = k_d VL - k_a VD$$

If at $t = 0$: $L = L_0$ and $D = 0$, above equation can be differentiated

$$L = L_0 e^{-k_d t}$$

$$D = \frac{k_d L_0}{k_a - k_d} (e^{-k_d t} - e^{-k_a t})$$



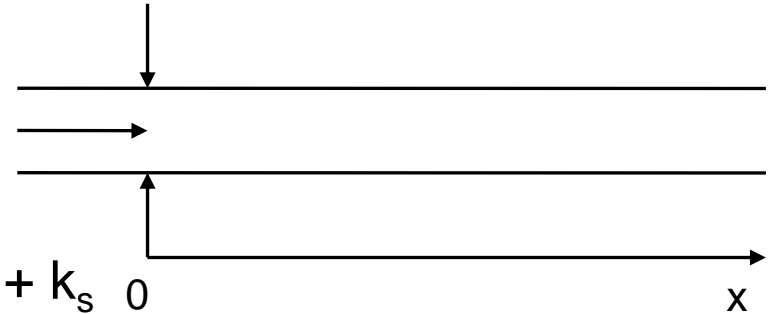
BOD decomposition process in (a) closed and (b) open system

POINTS SOURCE -STREETER-PHELPS EQUATION

A stream with a single-point source of BOD. The river segment is in a steady state and is characterized by plug flow with constant hydrological and geometry (PFR system). This is the simplest manifestation of the classic Streeter – Pheld model

Mass balance: $0 = -U \frac{dL}{dx} - k_r L$

$$0 = -U \frac{dD}{dx} + k_d L - k_a D \quad \text{v\o{r}i } k_r = k_d + k_s$$



If $L = L_0$ và $D = D_0$ at $t = 0$, then these equation can be solved for

$$L = L_0 e^{-\frac{k_r}{U} x}$$

$$D = D_0 e^{-\frac{k_a}{U} x} + \frac{k_d L_0}{k_a - k_r} \left(e^{-\frac{k_r}{U} x} - e^{-\frac{k_a}{U} x} \right)$$

POINTS SOURCE -STREETER-PHELPS EQUATION (cont)

❖ Some formulas calculate reaeration coefficient (k_a)

O'Connor-Dobbins (1956)

$$k_a = 3.93 \frac{U^{0.5}}{H^{1.5}}$$

Churchill (1962)

$$k_a = 5.026 \frac{U}{H^{1.67}}$$

Owens và Gibbs (1964)

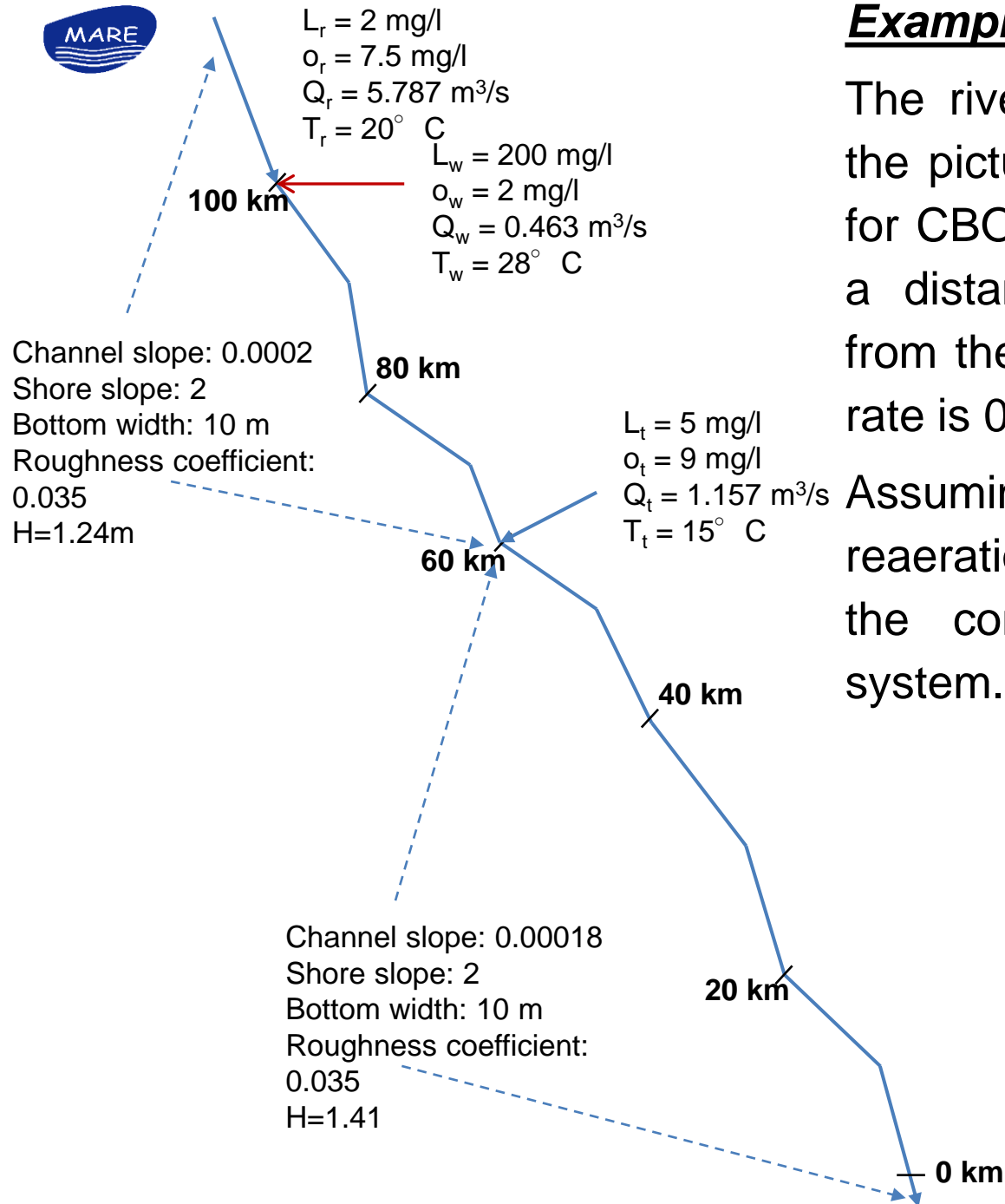
$$k_a = 5.32 \frac{U^{0.67}}{H^{1.85}}$$

where: k_a (1/day), U (m/s), H (m)

Example 1:

The river is described as shown in the picture. The de-oxygenation rate for CBOD is 0.5 day^{-1} in 20°C . From a distance of 20 km downstream from the plant, the CBOD deposition rate is 0.25 day^{-1} .

Assuming that O'Connor-Dobbins's reaeration formula is used, calculates the concentration of DO in the system.



The hydrographic morphological parameters and reaction kinetics of the system

Parameter	Units	KP > 100	KP: 100-60	KP < 60
Depth	m	1.19	1.24	1.41
Area	m ²	14.71	15.5	18.05
Flow	m ³ s ⁻¹	5.787	6.250	7.407
	m ³ d ⁻¹	500,000	540,000	640,000
Velocity	m s ⁻¹	0.393	0.403	0.410
	m d ⁻¹	33,955	34,891	35,524

Parameter	KP > 100	KP: 100 - 80	KP: 80 - 60	KP < 60
T (°C)	20	20.59	20.59	19.72
O _s (mgL ⁻¹)	9.092	8.987	8.987	9.143
k _a (d ⁻¹)	1.902	1.842	1.842	1.494
k _r (d ⁻¹)	0.50	0.764	0.514	0.494
k _d (d ⁻¹)	0.50	0.514	0.514	0.494

With a diffusion system such as an estuary the Streeter-Phelps equation can be written as:

$$0 = E \frac{d^2L}{dx^2} - U \frac{dL}{dx} - k_r L$$

$$0 = E \frac{d^2D}{dx^2} - U \frac{dD}{dx} + k_d L - k_a D$$

If $L = L_0$ và $D = D_0$ at $t = 0$, the solution for BOD is

$$L = L_0 e^{j_1 r x} \quad x \leq 0$$

$$L = L_0 e^{j_2 r x} \quad x \geq 0$$

ESTUARY STREETER-PHELPS MODEL (cont)

The solution to oxygen deficiency

$$D = \frac{k_d}{k_a - k_r} \frac{W}{Q} \left(\frac{e^{j_{1r}x}}{\alpha_r} - \frac{e^{j_{1a}x}}{\alpha_a} \right) \quad x \leq 0$$

$$D = \frac{k_d}{k_a - k_r} \frac{W}{Q} \left(\frac{e^{j_{2r}x}}{\alpha_r} - \frac{e^{j_{2a}x}}{\alpha_a} \right) \quad x \geq 0$$

where

$$L_0 = \frac{W}{\alpha_r Q}$$

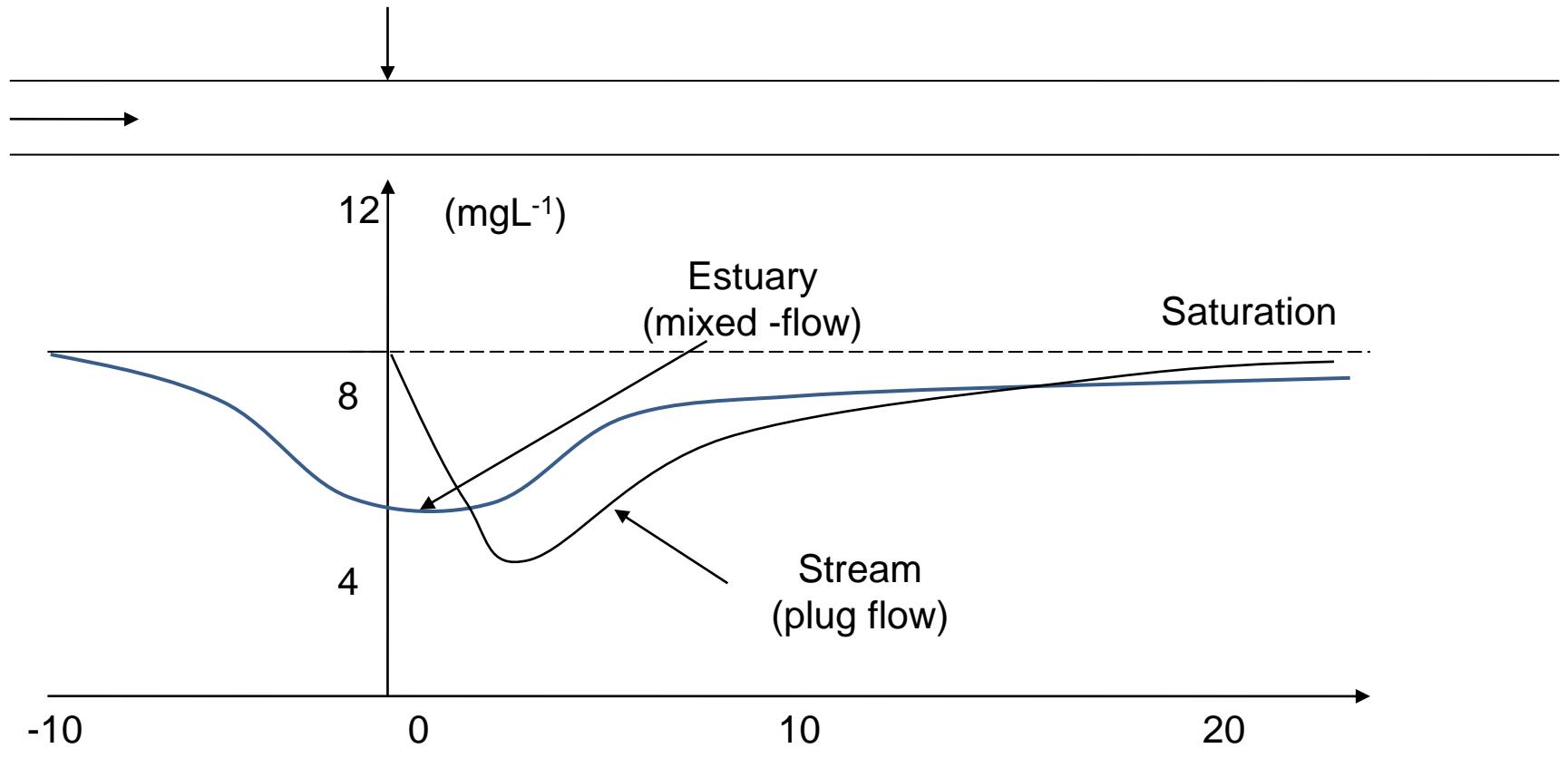
$$\alpha_r = \sqrt{1 + \frac{4k_r E}{U^2}}$$

$$\alpha_a = \sqrt{1 + \frac{4k_a E}{U^2}}$$

$$\begin{matrix} j_{1r} \\ j_{2r} \end{matrix} = \frac{U}{2E} (1 \pm \alpha_r)$$

$$\begin{matrix} j_{1a} \\ j_{2a} \end{matrix} = \frac{U}{2E} (1 \pm \alpha_a)$$

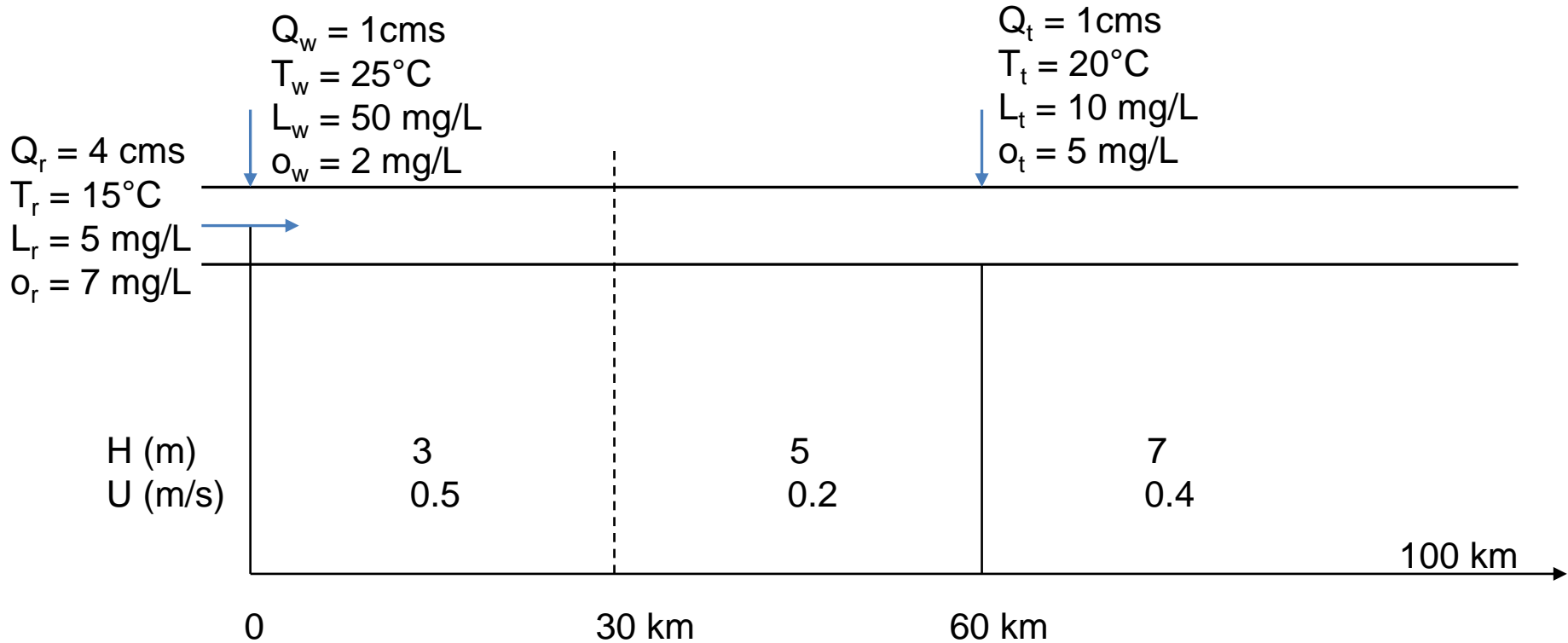
ESTUARY STREETER-PHELPS MODEL (cont)



DO chart for a point waste source into an estuary

Exercises 1: Determine BOD and DO for the following section of the river.

For the decomposition rate of BOD at 20°C is 0.35 (1/day), $\theta = 1.047$.



STRETER- PHELPS DISSTRIIBUTED SOURCES

PARAMETERIZATION OF DISTRIBUTION SOURCES

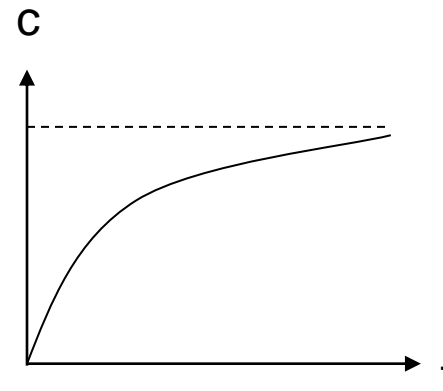
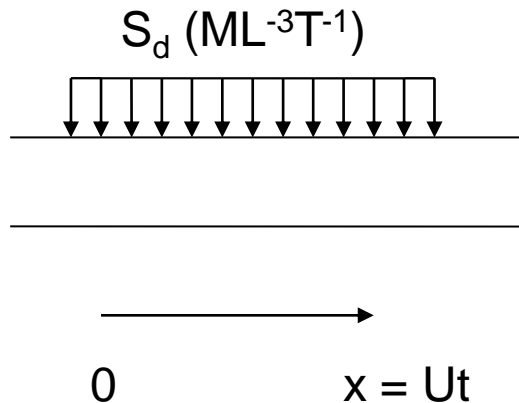
Mass balance in case of plug- flow: $0 = -U \frac{dc}{dx} - kc + S_d$

If at $t = 0$: $c = c_0$, then the solution is:

$$c = \frac{S_d}{k} (1 - e^{-kt})$$

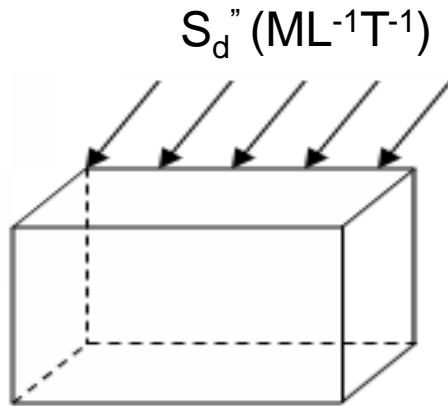
S_d = the rate of the distribution source. ($ML^{-3}T^{-1}$).

t = travel time , $t = x/U$.

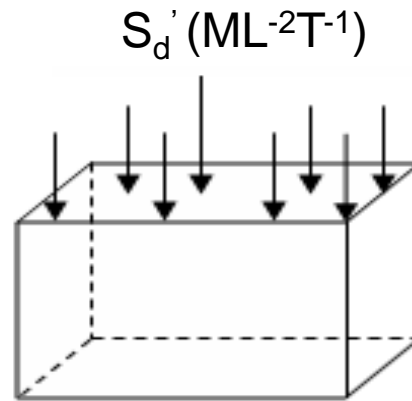


PARAMETERIZATION OF DISTRIBUTION SOURCES (cont)

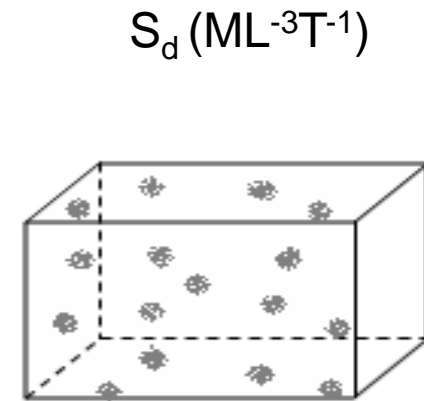
❖ Distributed source types



(a) Line load



(b) Area load



(c) Volume load

$$S_d = S_d'' \frac{L}{V} = \frac{S_d''}{A_c}$$

$$S_d = S_d' \frac{A_s}{V} = \frac{S_d'}{H}$$

L = distribution source length

V = volume

A_c = the cross-section area of the segment in which the source is included.

- ❖ Source: bottom sludge with high organic concentration

Mass balance:

$$0 = -U \frac{dL}{dx} - k_r L + S_L$$

Where S_L = the speed of the BOD distribution source ($\text{gm}^{-3}\text{d}^{-1}$)

k_r = rate of BOD removal (day^{-1}).

Solution when $t = 0$: $L = 0$:

$$L = \frac{S_L}{k_r} (1 - e^{-k_r t})$$

The mass balance for oxygen deficiency is written as follows

$$0 = -U \frac{dD}{dx} - k_a D + \frac{k_d}{k_r} S_L (1 - e^{-k_r t})$$

At $t = 0$: $D = 0$, The solution to mass balance is as follows:

$$D = \frac{k_d S_L}{k_r k_a} (1 - e^{-k_a t}) - \frac{k_d S_L}{k_r (k_a - k_r)} (e^{-k_r t} - e^{-k_a t})$$

Where $t =$ travel time. ($t = x/U$)

- ❖ Source: Plants (photosynthesis)
- ❖ Deposition: plants (respiration), SOD
- ❖ Mass balance

$$0 = -U \frac{dD}{dx} - k_a D - P + R + \frac{S'_B}{H}$$

Where P, R: the rate of photosynthesis and respiration of plants ($\text{gm}^{-3}\text{nday}^{-1}$)

S'_B = oxygen demand rate for sediment ($\text{gm}^{-2}\text{day}^{-1}$)

H = depth (m)

- ❖ The solution when $t = 0$: $L = 0$:

$$D = \frac{-P + R + (S'_B/H)}{k_a} (1 - e^{-k_a t})$$

- ❖ General solution to the points and distribution sources of BDO and DO.

- ❖
$$L = \boxed{L_0 e^{-k_r t}} + \boxed{\frac{S_L}{k_r} (1 - e^{-k_r t})}$$

↑ Point source ↑ Distribution source

Point deficit

Point BOD

$$D = \boxed{D_0 e^{-k_r t}} + \boxed{\frac{k_d L_0}{k_a - k_r} (e^{-k_r t} - e^{-k_a t})}$$

$$+ \frac{-P + R + (S'_B / H)}{k_a} (1 - e^{-k_a t})$$

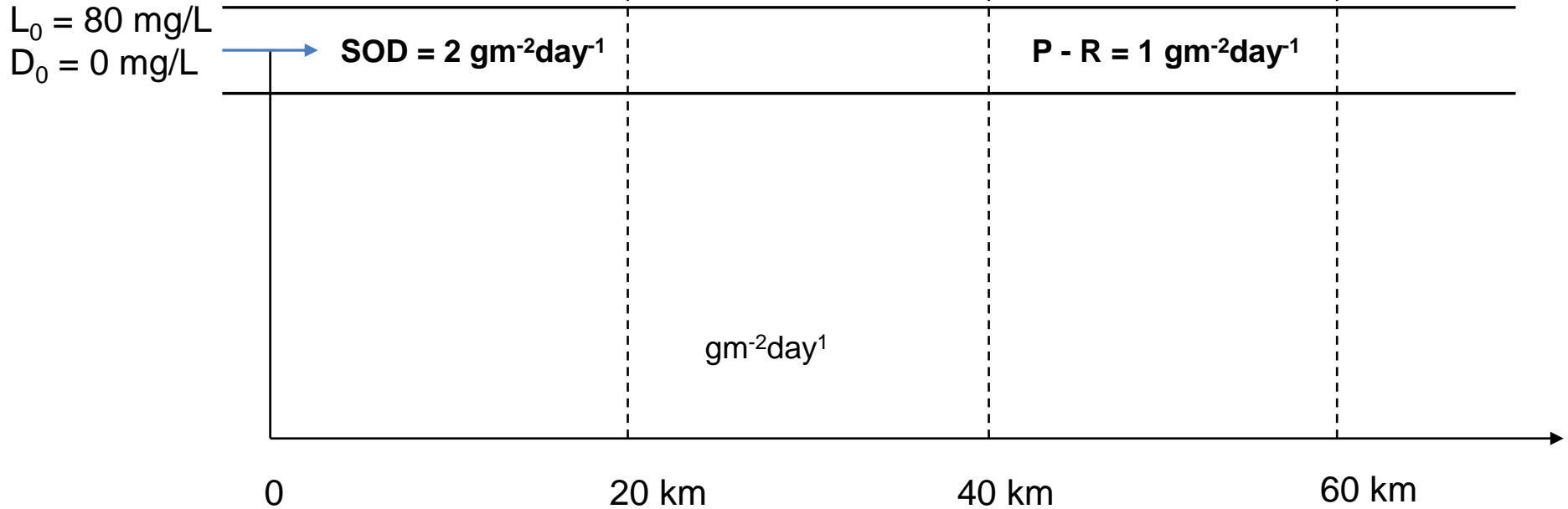
Distribution Deficit

$$+ \frac{k_d S_L}{k_r k_a} (1 - e^{-k_a t}) - \frac{k_d S_L}{k_r (k_a - k_r)} (e^{-k_r t} - e^{-k_a t})$$

Distributed BOD

Exercises:

Determine bod and do for the following section of the river.



U (mps)	0.1	0.15	0.1
H (m)	0.8	1	1
k_r (ngày ⁻¹)	0.2	0.1	0.1
k_d (ngày ⁻¹)	0.1	0.1	0.1
k_a (ngày ⁻¹)	1	1.2	1.2
o_s (mgL ⁻¹)	10	9	8